

Decolourization of Polyaluminium Chloride and Fungal Sequencing Batch Aerobic Reactor Treated Molasses Spentwash by Ozone

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Abstract Molasses spentwash from distilleries is characterized by high COD and color. The treatment of distillery spentwash by coagulation with polyaluminium chloride(PAC) followed by biological treatment with fungal sequencing batch aerobic reactor(FSBAR) resulted in 87% decolorization. To achieve further decolorization, ozonation of treated distillery spentwash was carried out at different ozone doses and contact times. It was found that pH had a negligible effect on decolorization. The optimum ozone dose was found to be 4.75 g/L at application rate of 3.8 g/h for 30 min with corresponding decolorization being 66%. The overall decolorization obtained by the combined treatment(PAC treatment, FSBAR and Ozonation) was 96% and the total COD removal was 81%.

Keywords COD Removal, Decolorization, Molasses Spentwash, Ozonation

1. Introduction

Distilleries generate large amount of spentwash that is of serious environmental concern. The spentwash is characterized by high chemical oxygen demand(COD), high biochemical oxygen demand(BOD), low pH, strong odour and dark brown colour[1,2]. Colour of spentwash is mainly due to melanoidins. The melanoidins are difficult to remove by conventional biological treatment such as anaerobic digestion and the activated sludge process[3]. However, fungal species have been reported for having potential to decolorize molasses spentwash[4]. Physical treatment like coagulation with Polyaluminium chloride(PAC) is also very effective in decolorization of DSW[5]. In the earlier studies by the authors, digested spentwash(DSW) was pretreated with polyaluminium chloride and fungal decolorization in a fungal sequencing batch aerobic reactor(FSBAR) was performed[6,7]. The total decolorization obtained after fungal treatment of PAC treated DSW was 87%.

Ozonation is used for decolorization of distillery spentwash in many studies. Oxidation by ozone could achieve 80% decolorization for biologically treated molasses wastewater with simultaneous 15-25% COD reduction. It also resulted in improved biodegradability of the effluent.

However, ozone only transforms the chromophore groups but does not degrade the dark coloured polymeric compounds in the effluent[8,9]. Ozone in combination with UV radiation enhanced spentwash degradation in terms of COD; however, ozone with hydrogen peroxide showed only marginal reduction even on a very dilute effluent[10]. Sangave et al.(2007) studied ozone and ultrasound as a pre-treatment step for the thermally pretreated spentwash for aerobic treatment by increasing the COD removal efficiency. Ozone was more efficient in COD removal with a 25-times increase in the rate of biodegradation of ozonated sample along with discoloration of the effluent sample[11].

In this paper, ozonation studies were carried out in order to investigate the effect of ozone on the COD and decolorization of PAC-FSBAR treated distillery spentwash.

2. Materials and Methods

2.1. Wastewater

Anaerobically digested spentwash(DSW) was obtained from a cane molasses based distillery situated near Mumbai, India. DSW was pretreated chemically with polyaluminium chloride(SVS chemical corporation, Pune, India) and then biologically in FSBAR.

pH, COD and color(absolute absorbance at 475 nm) of pretreated DSW used for ozone treatment were 3.42, 6400 mg/L and 1.43, respectively.

2.2. Experimental Setup

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The ozonation studies were conducted in a 28 cm long bubble column reactor of 6 cm diameter by varying the contact time at different ozone rates at room temperature. Ozone gas was generated using Ozone Generator (Model OZO 2 VTTL, Ozomax Inc., Quebec, Canada). The generator produced ozone by the corona discharge method using the oxygen as feed gas from an oxygen concentrator (Model 7F-5, Jiangsu Yuyue Medical Equipment Inc., China). The schematic of the experimental setup is shown in Figure 1. A rotameter with a regulating valve for flow adjustment was provided on oxygen concentrator and an output control scale was mounted in front of the generator assembly. Ozone generation was determined by measuring the gas flow rate after calibration. Ozone was supplied at the bottom of the reactor through a gas diffuser. Two ozone traps containing 2% potassium iodide solution were connected in series with the reactor in order to collect unreacted ozone.

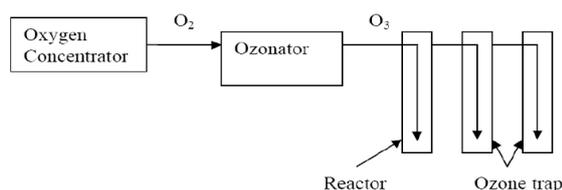


Figure 1. Schematic of the experimental setup

2.3. Ozonation Studies

The ozonation studies were conducted by varying the contact time at different ozone rate. All the studies were conducted in the laboratory at room temperature. 400 mL sample of the FSBAR effluent was filled in the reactor, which was connected serially with two ozone traps containing each 250 mL of 2% solution of aqueous potassium iodide. Ozone was bubbled through the aeration port of the reactor with the help of air diffuser. The ozone gas was allowed to react with the sample for a specific time interval and 5 mL sample were withdrawn at every 5 minutes. The samples were analyzed for COD and colour. The potassium iodide solutions from the ozone traps were titrated with sodium thiosulphate to determine the amount of unreacted ozone in the outlet stream. Knowing the amount of ozone concentration in the feed gas stream, the amount of ozone consumed in the reactor was calculated.

To determine the influence of the pH, pH was adjusted to the desired value (4, 6, 8, 10) by addition of sodium hydroxide to the wastewater and the applied ozone dose was kept constant at 6.3 g/h. Colour and COD were measured at every 5 minutes.

The ozonation reaction was done at 3.8, 5 and 6.3 g/h to know the effect of ozone dose on decolourization and COD removal.

For colour measurement, 5 mL samples were centrifuged at 8,000 rpm for 10 minutes. The supernatant after centrifugation was diluted 10 times for colour reduction measurement. The absorbance was measured at 475 nm using

Thermo Spectronic visible spectrophotometer. The decolourization yield was expressed as the percentage decrease in absorbance at 475 nm related to the initial absorbance at the same wavelength.

Chemical oxygen demand (COD) was determined based on the Standard Methods for Examination of Water and Wastewater [12].

3. Results and Discussion

Studies were carried out in order to investigate the effect of ozone on the decolourization and COD reduction of FSBAR treated distillery spentwash and results obtained are discussed in following sections.

3.1. Influence of pH

Influence of pH was studied for maximum decolourization of FSBAR treated effluent. At low pH, ozone exclusively react with compounds with specific functional groups through selective direct reactions such as electrophilic, nucleophilic or dipolar addition reactions [13]. Under basic pH, the hydroxide ions catalyze the decomposition of ozone to yield highly reactive and non-selective hydroxyl radicals, which have an oxidation potential higher than that of ozone [14].

The original pH of treated effluent was about 3.42. The pH was varied between 4 and 10 in different experiments to study the influence of initial pH. Figure 2 shows the variation of decolourization with time at different pH. The decolourization after 30 min of ozonation at all pH was 68-70%. This shows that the decolourization of FSBAR treated DSW was independent of pH. Figure 3 shows COD reduction at different pH. The COD reduction at pH 10 was faster than those at other pH. The final COD reduction at all the pH was 37.5%. The low difference in decolourization and COD reduction at various pH indicates that direct reactions of ozone with wastewater organics predominated to radical reactions.

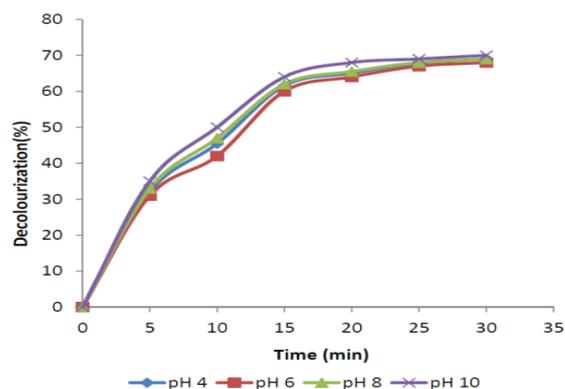


Figure 2. Decolourization of FSBAR treated effluent at various pH.

Coca *et al.* (2005) also studied the influence of pH during ozonation of spentwash [14]. The decolourization and COD reduction efficiencies at different pH were found similar.

As decolourization was not influenced by pH, all subse-

quent studies were done without any pH correction.

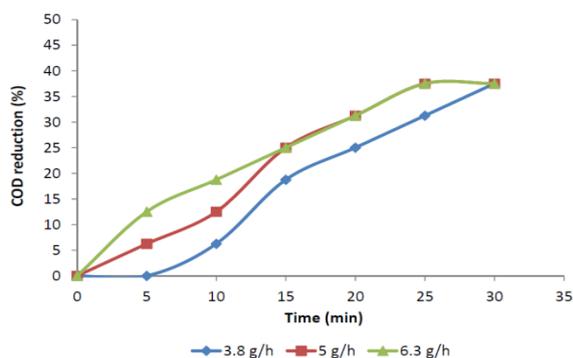


Figure 3. COD reduction of FSBAR treated effluent at various pH.

3.2. Effect of Ozone Dose

Ozone application rate was varied from 3.8 to 6.3 g/h to assess the effect of the applied ozone dosage on decolourization and COD removal.

3.2.1. Decolourization

Figure 4 shows the evolution of decolourization with the reaction time for experiments carried out at different ozone dosages. As a result of ozonation, absorbance at 475 nm decreased significantly. It reduced from the initial value of 1.43 to 0.48 at 3.8 g/h ozone dose and reduced to 0.45 in the case of 5 g/h and 6.3 g/h ozone doses. The maximum decolourization obtained was 69%. 4.75 g/L was found out to be optimum dose at applied ozone rate of 3.8 g/h for 30 min. Wastewater decolourization occurred mainly at the initial stage of the reaction (i.e. within 20 min of reaction). Melanoidins have conjugated carbon-carbon double bonds in their structure that are responsible for the brown colour [15]. The colour removal was probably due to the fact that ozone was able to cleavage these conjugated carbon-carbon double bonds.

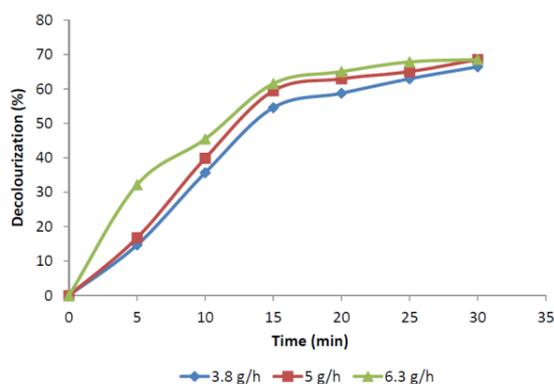


Figure 4. Decolourization of FSBAR treated effluent at various ozone doses.

Pena et al.(2003) studied the ozonation of biologically pretreated molasses spentwash by varying the dose from 1.6 g/h to 11.5 g/h. The decolourization achieved at various doses varied from 71% to 93% [16].

3.2.2. COD Removal

Figure 5 shows COD removal with the reaction time for experiments carried out at different ozone dosages. Maximum COD reduction of 37.5% was obtained at all the ozone dosage after 30 min of reaction. The efficiencies achieved were much lower than those reached in decolourization. The less COD removal may be due to the colour compounds present in wastewater. These compounds react with ozone, leading to organic compounds which might still demand oxygen until their final degradation.

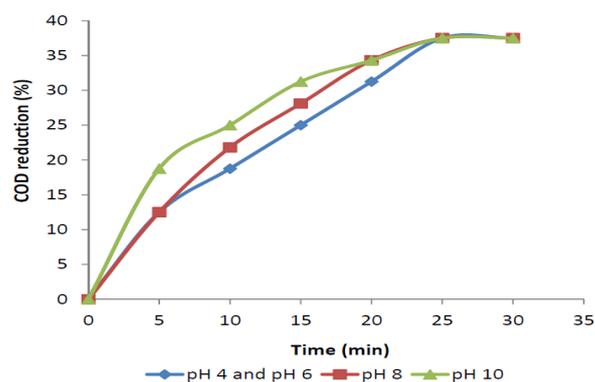


Figure 5. COD reduction of FSBAR treated effluent at various ozone doses.

Carboxylic acids have been indicated as products of melanoidin ozonation [15]. The reactivity of carboxylic acids with ozone has reported to be negligible [17]. It was observed by Arai et al. (1986) that the ozonation of humic substances also led to the formation of small molecules, mainly aldehydes (formaldehydes, acetaldehydes, glyoxal and methylglyoxal) and carboxylic acids (formic, acetic, oxalic, glyoxylic, pyruvic and ketomalonic acids) which accumulated in the solution due to their resistance towards further degradation by ozonation [18].

Pena et al. (2003) found that the ozonation of biologically pretreated molasses spentwash resulted in a COD reduction of 15% to 25% for the ozone dosage of 1.6 g/h to 11.5 g/h after 30 min reaction time [16].

3.2.3. Variation in pH

The initial pH of the wastewater was 3.42. Ozonation was carried out without modifying the pH of the FSBAR treated effluent. Ozonation process led to a slight drop in the pH value of the wastewater to 3.1, 3.08 and 3.07 for the ozone dosage of 3.8 g/h, 5 g/h and 6.3 g/h at the end of 30 min. This decrease in pH was due to formation of the acidic degradation products like carboxylic acids due to ozonation of melanoidin compounds [15].

3.2.4. Ozonation Efficiency

This parameter represents the yield of ozone consumption and is defined as the ratio of ozone consumed and the ozone supplied in the reactor after a given time [10]. The efficiency values at different ozone dose after 30 min of reaction are summarized in Table 1. Maximum ozonation efficiency of 76% was observed at applied ozone dosage of 3.8 g/h. The ratios between colour (absorbance at 475 nm)

removed and grams of ozone fed into the reactor after 30 min of reaction are also summarized in Table 1. An increase in the applied ozone dosage yielded a reduction in the above defined ratio, thus, low ozone dose (3.8 g/h) was enough to oxidize coloured compounds efficiently. Greater ozone dosages did not enhance the ratio and ozone left the reactor without being consumed by decolourization reactions.

Table 1. Effect of Ozone Dosage on Ozone Efficiency and Colour Removal.

Ozone dosage (g/h)	Ozone supplied (mg)	Ozone consumed (mg)	Ozonation efficiency (%)	Colour removed (A_{475}) / g ozone supplied
3.8	1922.4	1463.5	76	0.49
5	2383.2	1627.6	68	0.41
6.3	3193.2	1710.3	54	0.31

4. Conclusions

Ozonation was done on FSBAR effluent for decolourization. It was found that pH had a negligible effect on decolourization. Ozonation was performed at different ozone doses. 4.75 g/L was found out to be optimum dose at applied ozone rate of 3.8 g/h for 30 min. The decolourization of 66% was obtained at this dose. The total decolourization obtained by the combined treatment (PAC treatment, FSBAR and Ozonation) was 96% and the total COD removal was 81%. This shows that ozonation can be used effectively as tertiary treatment after fungal decolourization of digested distillery spentwash.

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